



Methanol Synthesis from CO₂

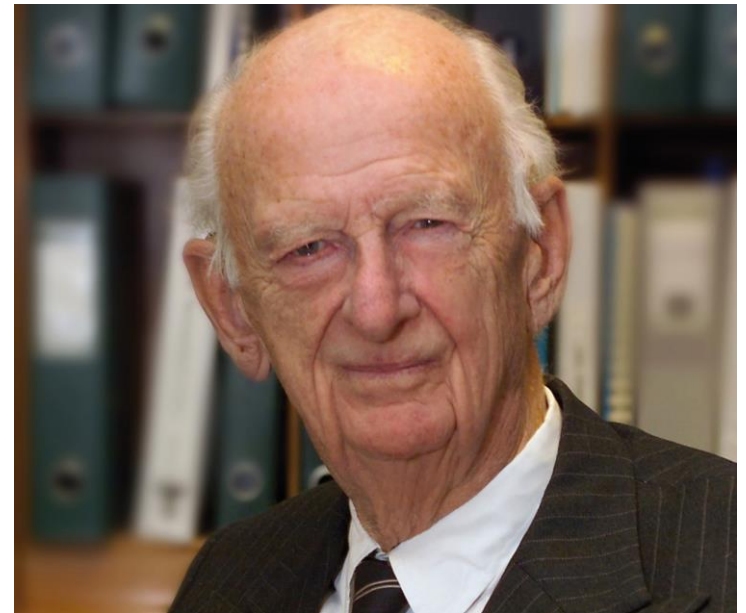
RESEARCH | TECHNOLOGY | CATALYSTS

[John Bøgild Hansen](#) - Haldor Topsøe

Columbia University, New York City – April 14, 2014

We have been committed to catalytic process technology for more than 70 years

- Founded in 1940 by Dr. Haldor Topsøe
- Revenue: 700 million Euros
- 2700 employees
- Headquarters in Denmark
- Catalyst manufacture in Denmark and the USA



Topsoe Fuel Cell A/S

- Founded in **2004** after more than 20 years of research and development
- Located in Lyngby, **Denmark** (north of Copenhagen)
- Employees 105
- Development, manufacturing and marketing of the **Solid-Oxide Fuel Cell** technology (SOFC technology)
- Subsidiary of **Haldor Topsøe A/S** (100%)



Topsoe Fuel Cell Employees



Headquarters in Lyngby, Denmark



Supported by funding under the
LIFE Programme
of the European Union



Methanol synthesis

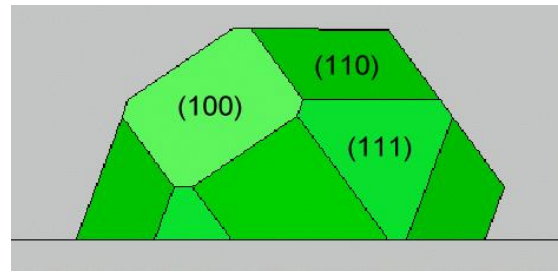
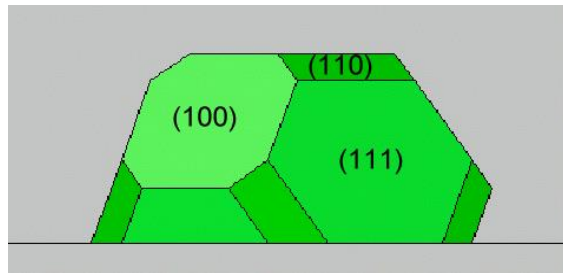
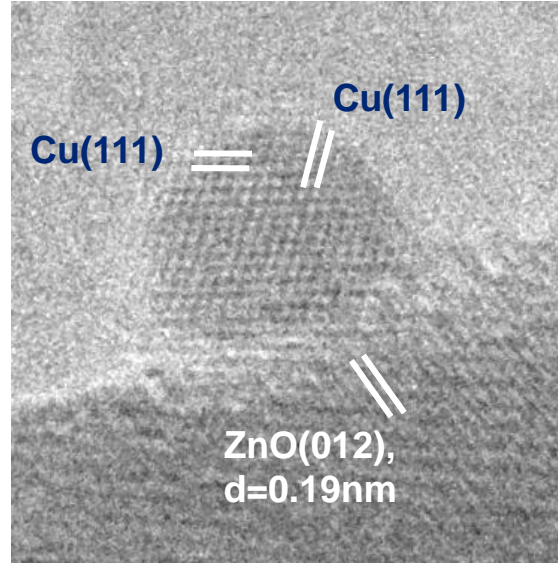
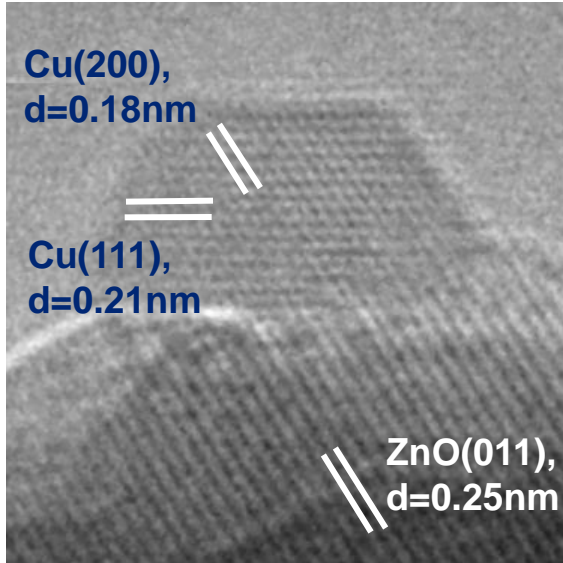
- $\text{CO} + 2\text{H}_2 = \text{CH}_3\text{OH} + 91 \text{ kJ/mol}$
- $\text{CO}_2 + 3\text{H}_2 = \text{CH}_3\text{OH} + \text{H}_2\text{O} + 41 \text{ kJ/mol}$

$$M = \frac{H_2 - \text{CO}_2}{\text{CO} + \text{CO}_2} = 2$$

The Active Site of Syngas Catalyst

H_2

H_2/H_2O



1.5mbar, 220°C

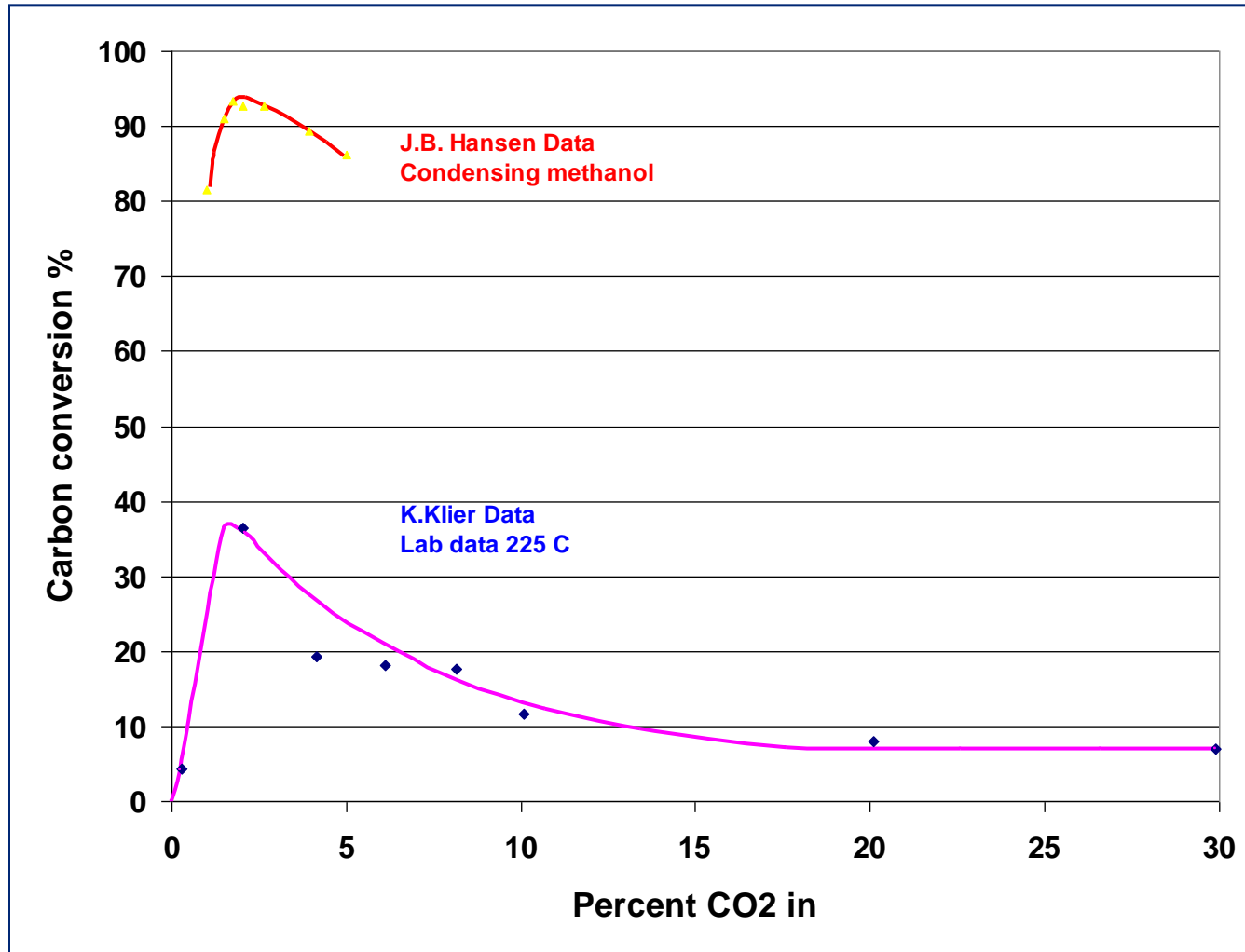
1.5mbar, $H_2/H_2O=3/1$, 220°C

Cu is metallic when catalyzing:

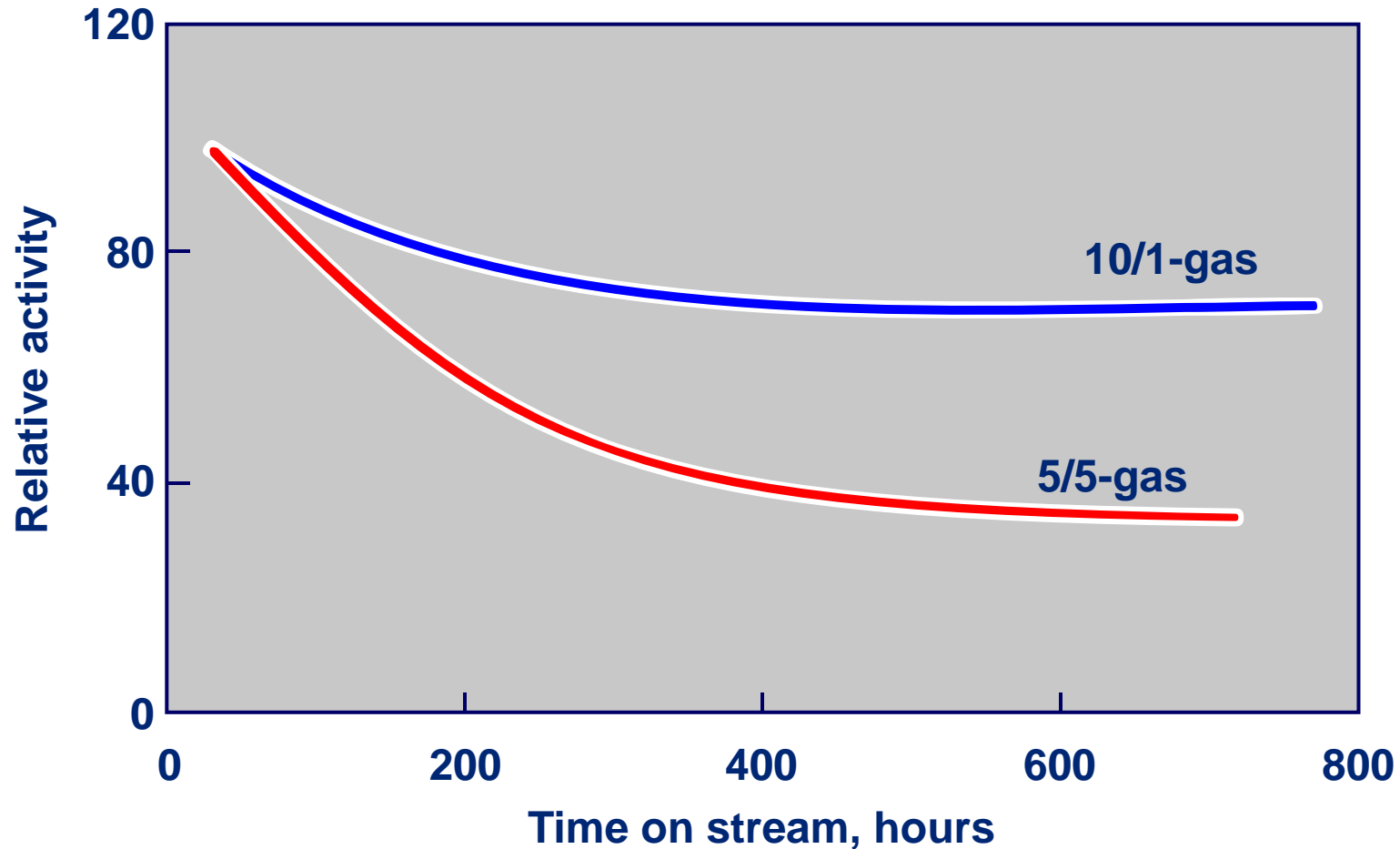
- WGS
- MeOH synthesis
- MeOH reforming

Catalyst dynamic:
- Number of active sites depends on conditions

Conversion of methanol as function of CO₂ content in stoichiometric gas



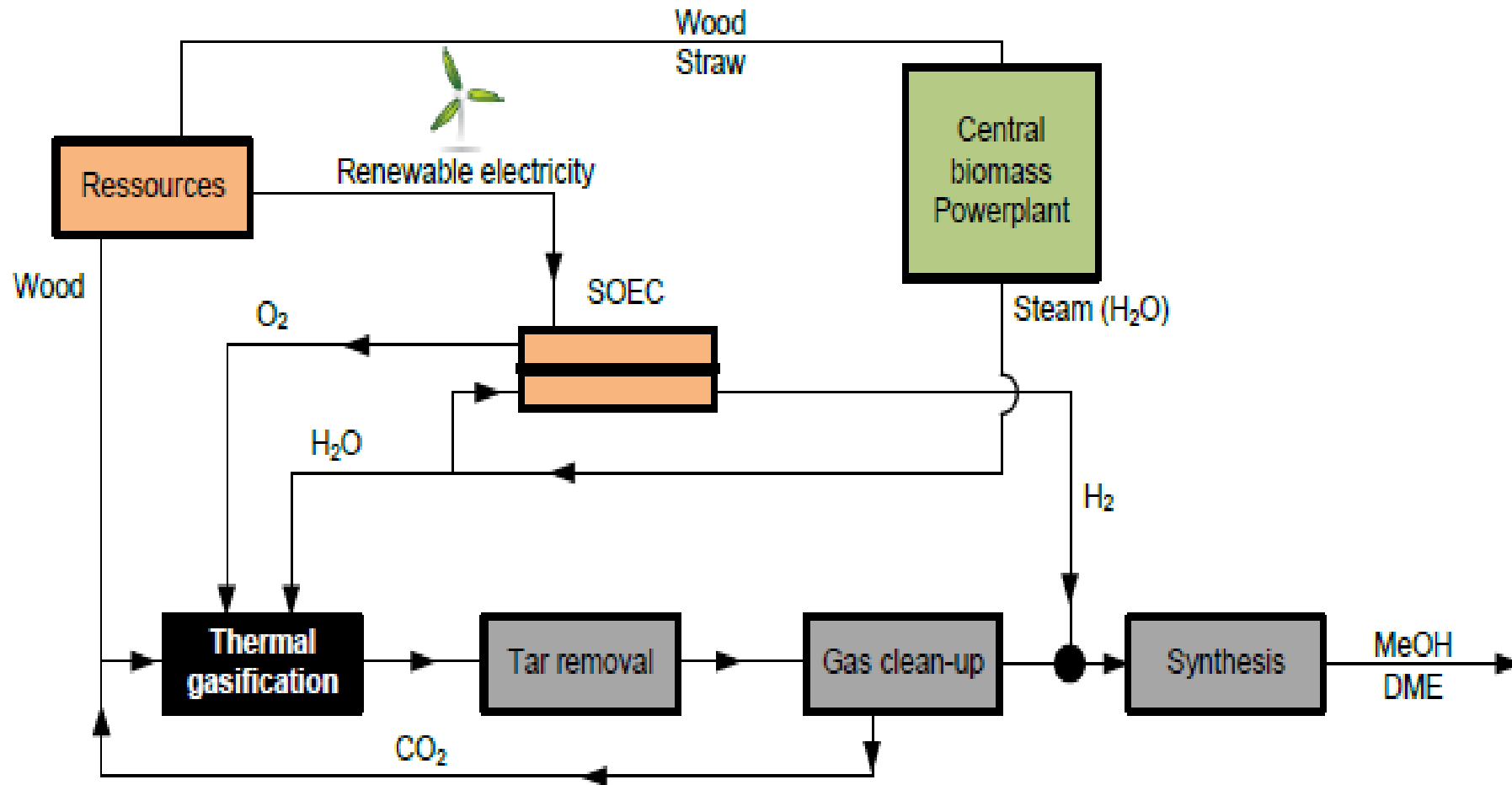
Ageing of methanol catalyst in Normal and Dry Syngas



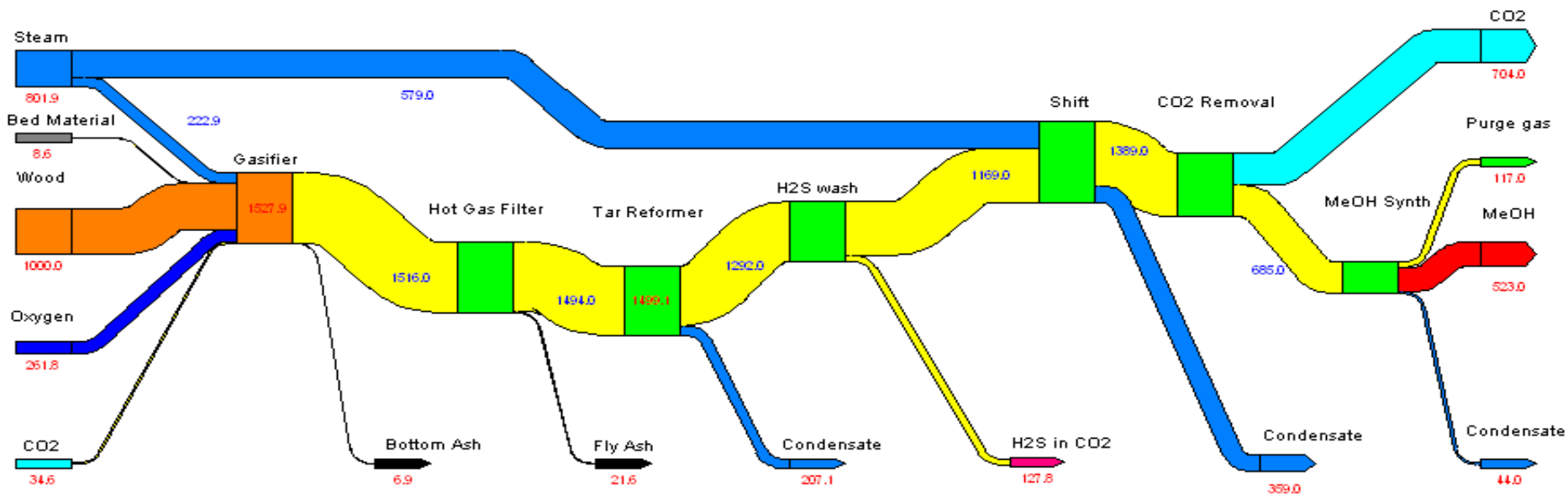
Reformers for Methanol Plant utilising CO₂



GreenSynFuel Project



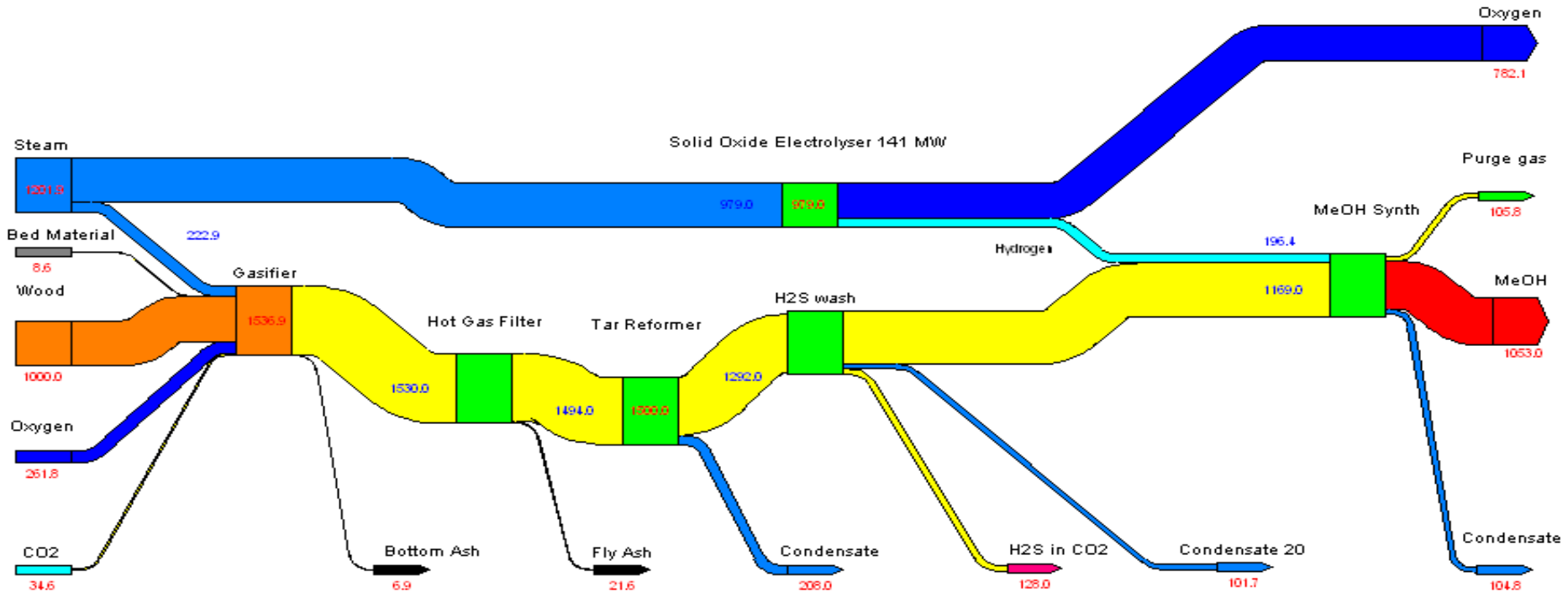
Mass Flows in Wood to MeOH



Mass balances for Wood Gasification to MeOH

Flows in Metric Tons per day

Mass Flows in Wood + SOEC to MeOH



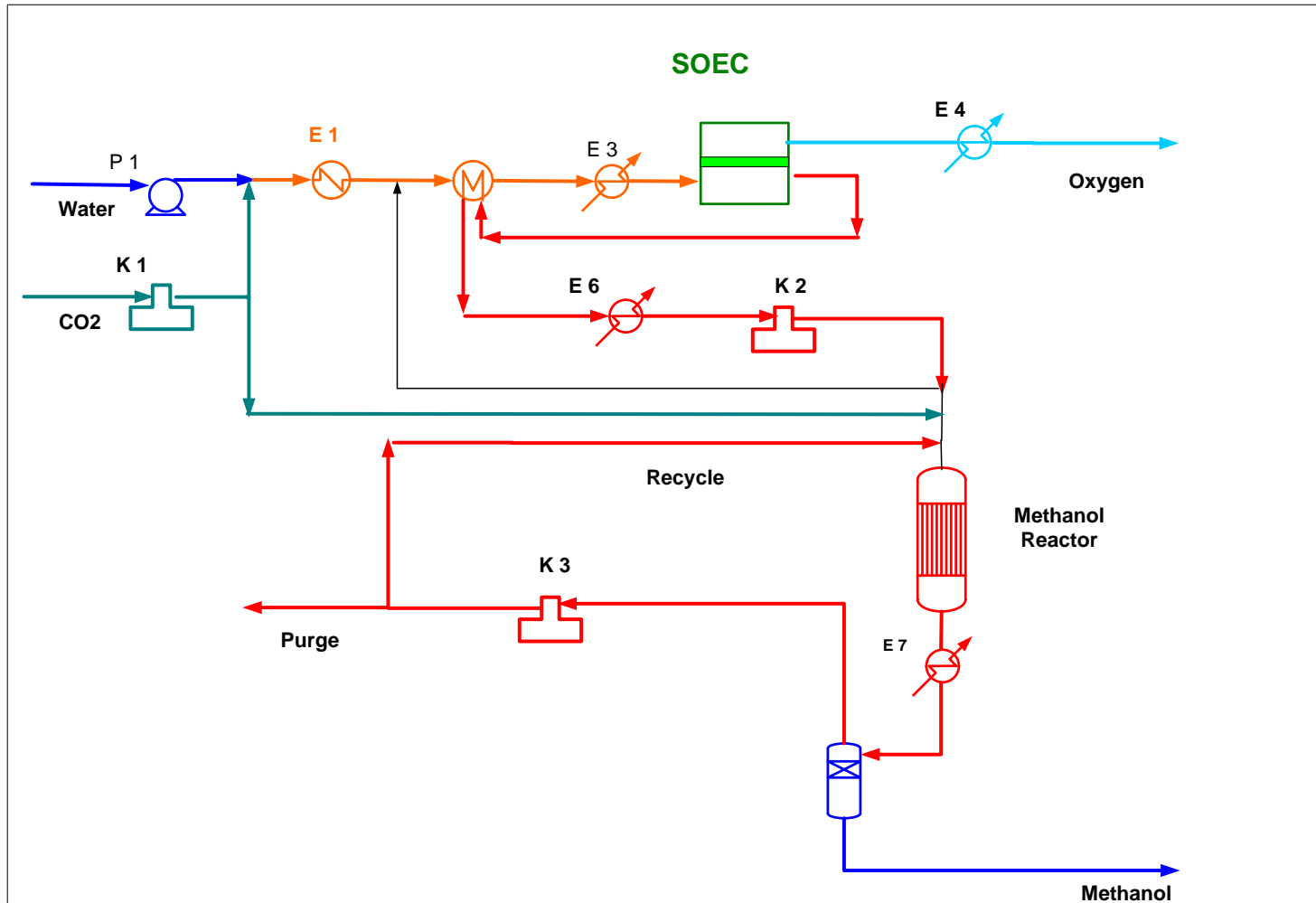
Mass balances for combined Wood Gasification and SOEC to MeOH

Flows in Metric Tons per day

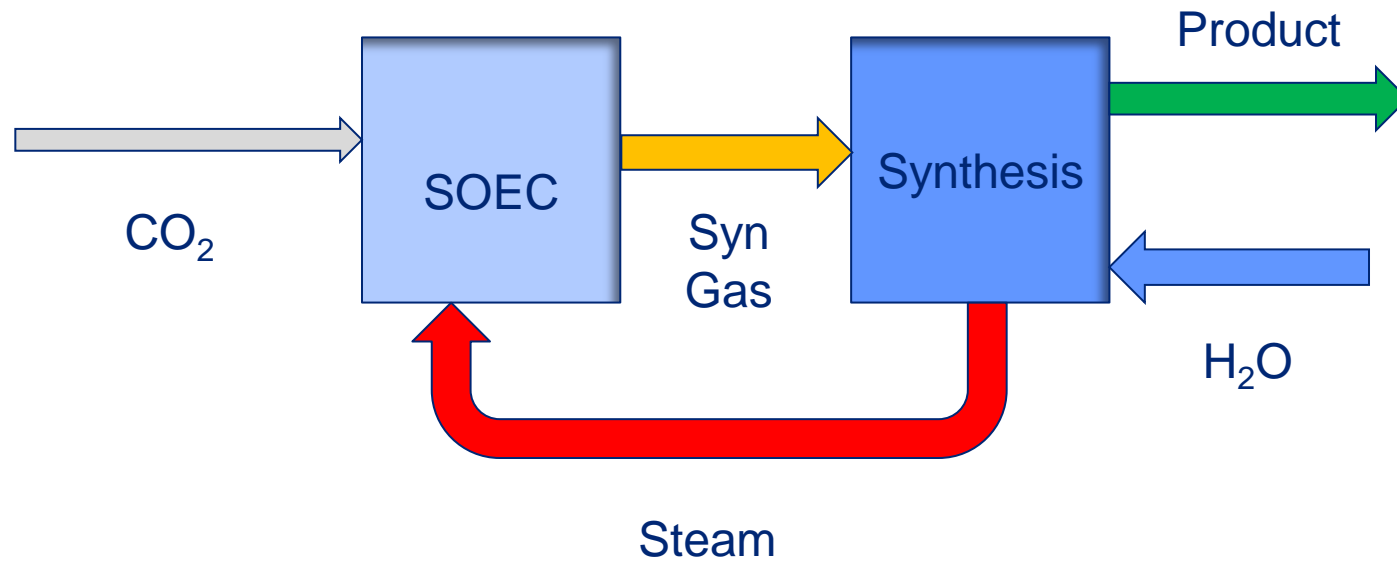
Efficiencies: Stand alone wood gasifier and gasifier plus SOEC

LHV Efficiency %	Wood Gasifier alone	Wood gasifier Plus SOEC
Methanol	59.2	70.8
District Heat	22.6	10.8
Total	81.8	81.6

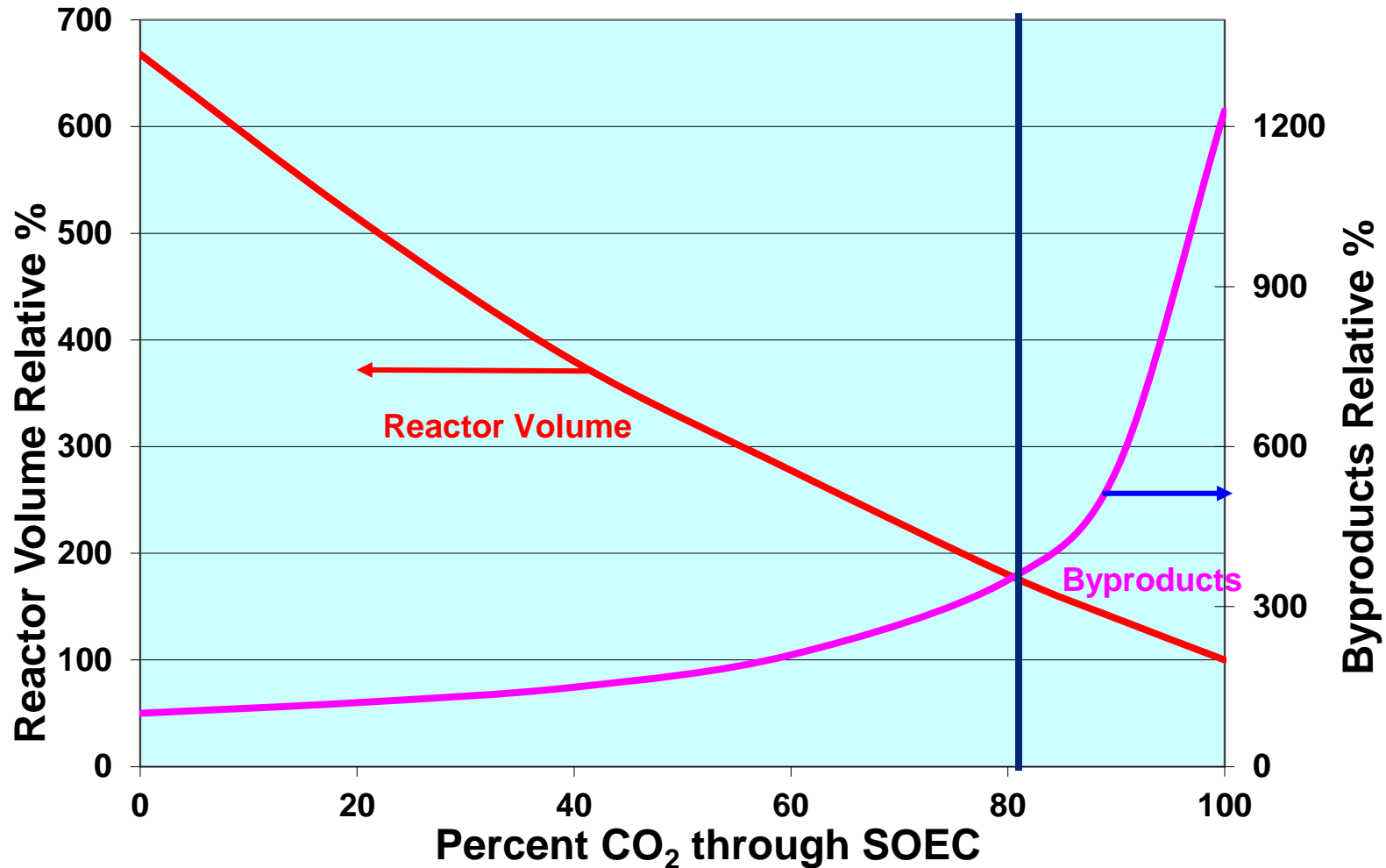
Methanol from CO₂ and Steam



Synergy between SOEC and fuel synthesis



Reactor volume and byproducts as function of CO₂ converted in SOEC



Results of "to pressurize SOEC stacks or not"

<i>SOEC Pressure</i>	<i>Syngas Comp %</i>	<i>CO2 Comp</i>	<i>LHV Efficiency %</i>
Atmospheric	6.8	0.1	75.8
@50 bar	0.0	1.9	79.5
<i>Max. theoretical</i>			83-88

Conclusions

- Very efficient methanol plants based on power, steam and CO₂ is possible via SOEC
- Co-electrolysis offers the opportunity to reduce methanol synthesis catalyst volumes by a factor around 5
- Pressurising the SOEC stacks can eliminate synthesis gas compressor and increase efficiency
- Coupling SOEC with biomass gasification can double the biomass potential by converting excess carbon.