Simultaneous measurement of CO2 sorption and swelling of phosphate-based ionic liquid

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Abstract

The development of alternative CO2 capture solvents such as ionic liquids (ILs) and nanoparticle organic hybrid materials (NOHMs) have provided interesting options for CO2 capture. In this study, CO2 interactions with 1,3-dimethylimidazolium dimethylphosphate ([MMIM]DMP), 1-ethyl-3-methylimidazolium dimethylphosphate ([EMIM]DMP) and 1-ethyl-3-methylimidazolium diethylphosphate ([EMIM]DEP) that contain inorganic ester groups based on phosphate, were investigated using ATR FT-IR spectroscopy. CO2-induced swelling, CO2 diffusivity and CO2 capture capacity were simultaneously measured to identify CO2 capture mechanisms, kinetics and diffusion behaviors as a function of the alkyl chain length of the cation. Henry's law constants of CO2 were found to be in the range of 4–11 MPa, which is in agreement with those reported in other studies.

Keywords: CO2 capture; ATR FT-IR spectroscopy; Ionic liquids; Mechanism; Diffusivity

1. Introduction

Carbon capture and storage (CCS) is one of the most difficult environmental problems with unprecedented scale. Capturing CO2 from large point sources has become a global and urgent issue since the escalating atmospheric concentration of CO2 is threatening the delicate balance on Earth. The conventional technology to capture CO2 is chemical absorption using amine-based solvents. While offering fast kinetics and high CO2 capture capacities, amine scrubbing still faces a number of challenges including a high energy demand, the degradation of the amine, the release of volatile organic compounds, and the risk of equipment corrosion. Room temperature ionic liquids (RTILs) have been considered as promising alternative solvents to address some of these challenges of amine scrubbing [1–4]. RTILs possess many attractive properties, such as non-flammarbility, high thermal stability, wide electrochemical window, and tunable properties via the combination of different cations and anions [5–8]. One of the main reasons to use ILs for CO2 capture lies in their negligible vapor pressure, which decreases the risk of worker exposure and that of material loss. Additionally, compared to the amine-based reagents, which utilize strong chemical interactions with CO2 by forming carbamate species, the separation of CO2 through physical interaction is particularly attractive because the stripping of CO2 from a RTIL can be operated under much milder conditions thereby reducing the overall operation cost.

Several recent studies have reviewed the main aspects of the use of RTILs for CO2 capture [9–14]. Cadena et al.
investigated the effect of anions in alkylimidazolium-based ILs for CO2 capture via experimental and molecular simulation studies. They revealed that the anions play a critical role in interacting with CO2 because anions containing fluorine exhibit a high affinity toward CO2 [9]. Anthony et al. observed that [BMIM]Tf2N exhibited relatively high capacity for CO2 while [BMIM]BF4 and [BMIM]PF6 had lower affinity for CO2 [10]. Brennecke et al. investigated the effect of anions and cations in imidazolium-based ILs on the solubility of CO2. Results showed that solubility of CO2 in [BMIM]-based ILs is strongly dependent on the choice of the anion and increases in the following order: [NO3] < [TfO] < [DCA] < [BF4] ~ [PF6] < [Tf2N]. Additionally, they observed that an increase in the alkyl chain length of the cation increases the CO2 solubility marginally [11].

Despite these findings, there is still a long path ahead to find suitable material candidates that are competitive, both from economic and technological viewpoints, compared to currently available processes such as the widely used amine-based solvents [15]. Brennecke et al. found that it was difficult to employ the task-specific ILs in industrial applications due to the increasing viscosity after the absorption reaction [8]. Wasserscheid et al. have found that the presence of halogen atoms in typical ionic liquids containing anions (such as [AlCl4]−, [PF6]−, [BF4]−, [TfO]− or [Tf2N]−) may cause serious concerns if the hydrolysis stability of the anion is poor (e.g. for [AlCl4]− and [PF6]−) or if a thermal treatment of spent ionic liquids is desired. They have recently anticipated that ionic liquids containing alkylsulfonate or alkylsulfate anions are better options from an environmental perspective than ionic liquids containing anions with fluorine atoms, such as hexafluorophosphate or bis(trifluoromethanesulfon)ylamides [16].

The ILs with alkyl-substituted imidazolium cation and dialkylphosphate anions can be synthesized using a one-pot method with high yield, low cost and ease of purification [17–19]. Compared with the chloride-based ionic liquids, alkyl phosphate anions have sufficiently high hydrogen bond basicity and lower viscosities [20]. Especially, this kind of ILs with an inorganic ester group might exhibit a high affinity toward CO2. To the best of our knowledge, CO2 capture mechanisms in ILs with alkyl-substituted imidazolium cations and dialkylphosphate anions, has never been studied so far. In this work, CO2 capture mechanisms of this kind of ILs deprived of fluorinated anions — i.e. [MMIM]DMP, [EMIM]DMP and [EMIM]DEP — were investigated using an ATR FT-IR spectroscopy method developed in prior studies [21,22]. In addition, the swelling behaviors of the three ILs as a result of CO2 absorption were investigated.

2. Experimental

2.1. Materials

[MMIM]DMP, [EMIM]DMP and [EMIM]DEP with a purity of 98.0% were supplied by Fisher scientific Co., and were used without further purification. Prior to testing, the materials were degassed and dried under vacuum for 12 h at 353.15 K. A little weight difference was observed before and after pretreatment. Samples obtained after pretreatment were characterized by 1H NMR and 13C NMR spectra, and no extra peak was found. The structures of the ILs are shown in Table 1. High-purity anhydrous carbon dioxide with a purity of 99.999% was obtained from Tech Air Co.

2.2. Apparatus and procedure

2.2.1. Attenuated total reflectance (ATR) FT-IR spectroscopy

In order to measure the CO2 capture capacity and swelling behaviors of the ILs, and then analyze the absorption mechanisms, a Fourier-transform infrared (FT-IR) spectrometer (Nicolet 6700, Thermo Fisher Scientific Inc.) equipped with a deuterated triglycine sulfate (DTGS) detector, an attenuated total reflectance (ATR) accessory topped with a high-pressure fluid cell (Golder Gate™ Supercritical Fluids analyzer, Specac Ltd. (UK)) and a PID temperature controller was used in this study.

2.2.2. Measurement of CO2 capture capacity and thermally-induced swelling

The CO2 capture capacity and thermally-induced swelling were measured as described in prior studies [21]. Typically, a small amount of sample was deposited onto the surface of the diamond crystal, which was then heated to the desired temperature. Then the sample cell was pressurized with CO2. The spectra were collected in the range 4000 cm−1−500 cm−1 from the acquisition of 32 scans, with a resolution of 2 cm−1.

Table 1

<table>
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<tr>
<th>Ionic liquid</th>
<th>Structure</th>
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<tr>
<td>1-Ethyl-3-methylimidazolium dimethylphosphate ([EMIM]DMP)</td>
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<tr>
<td>1-Ethyl-3-methylimidazolium 3-diethylphosphate ([EMIM]DEP)</td>
<td><img src="image3.png" alt="Structure" /></td>
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</table>
All samples reached equilibrium within 10 min, and the experiments were repeated at least twice under each temperature and pressure condition. The measurements were conducted from 0 to 4.83 MPa at either 298.15 K, 303.15 K or 313.15 K.

2.2.3. Measurement of CO₂ diffusivity

CO₂ diffusivity in ILs was also measured using ATR FT-IR spectroscopy equipped with a high pressure sample cell. Typically, a thin layer of sample was deposited on top of the diamond crystal. The temperature was set at 298.15 K and the thickness of the layer was measured using a caliper. The spectrum of the sample was then collected using the same acquisition parameters as described above. Afterwards, the sample cell was pressurized with CO₂ at 1.38 MPa. Spectra were then collected every 3 s up to reaching equilibrium. The CO₂ and IL absorbance bands were well resolved and did not require deconvolution techniques for spectral analysis. The CO₂ (2370–2310 cm⁻¹) absorbance band was integrated using a two-point base line correction.

3. Thermodynamic background

3.1. Calculation of CO₂ capture capacity and CO₂-induced swelling

The CO₂ capture capacities were determined from the ATR FT-IR spectroscopy measurements as described in prior studies [20]. Beer–Lambert law expresses the relationship between absorbance (A), absorptivity (ε), concentration (c), and effective thickness of the evanescent wave (dₙ) [23]:

\[ A = ε \cdot c \cdot dₙ \]  (1)

The refractive index of ionic liquids (n_[MIM]DMP = 1.486, n_[MMIM]DMP = 1.483 and n_[EMIM]DMP = 1.475) was used to calculate dₙ as described in Ref. [23]. The absorbance of CO₂ was quantified by measuring the intensity of the stretching band around 2338 cm⁻¹. The molar absorptivity of CO₂ (ε) at high-pressure was considered equal to 1.0 × 10⁶ cm²/mol [24].

The degree of swelling (S) is defined as a ratio of the change of the solvent volume over the initial volume [25]:

\[ S = \frac{A^0 \cdot dₙ}{A \cdot dₙ^0} - 1 \]  (2)

Sakellarios et al. already used this method to study the high-pressure CO₂-induced swelling of ILs [26]. Here, the absorbance of C-O stretching band around 1040 cm⁻¹ from the ether groups of the ILs was used to calculate the swelling. This band was selected because it is relatively well-isolated from other bands and therefore does not require major deconvolution treatment. Because of the relative broad band of C-O, the swelling ratios obtained via the integration in the interval from 1075 cm⁻¹ to 950 cm⁻¹ would more likely represent the volume change of ILs. In this calculation, the absorptivity was assumed constant regardless of CO₂ concentration in the sample. The absorptivity is involved in the calculation of the effective thickness [25], and therefore it resulted that the effective thickness was considered constant in the pressure range studied. Combining Eqs. (1) and (2), the CO₂ capture capacity in moles of CO₂ per gram of absorbent (m) can be determined as follows:

\[ m = \frac{c}{M_x} \times 1000 \]  (3)

Through m obtained above, the CO₂ solubility in mole fraction basis (x) can be further calculated using the following equation:

\[ x = \frac{m}{1000/M_{IL}} \]  (4)

3.2. Gas–liquid phase equilibrium

The condition for the phase equilibrium is satisfied when the fugacities of the gas component have equal values in both phases at a constant temperature and pressure:

\[ f^e_g = f^e_l \]  (5)

Due to the negligible vapor pressure of ILs, the gas phase is assumed to be pure CO₂. The fugacity of the pure carbon dioxide in gas phase can be expressed as the product of the total pressure (P) and the fugacity coefficient (φ₁). Therefore, the gas–liquid equilibrium expression is as follows:

\[ f^e_g = P_1 \varphi_1 \]  (6)

The fugacity coefficient of CO₂, φ₁, in Eq. (6) can be calculated using Span–Wagner equation of state. In contrast to the gas-phase fugacities, liquid-phase fugacities depend slightly on the pressure at constant temperature (T) and pressure:

\[ f^e_l(P) = f^e_l(P_0) \exp \int_{P_0}^{P} \frac{1}{V_1(RT)^{-1}} dP \]  (7)

The solubility data of CO₂ in ionic liquids can be correlated using the Krichevsky–Kasarnovsky (K–K) equation, which does not take into account the non-ideality of the solute in the liquid phase:

\[ \ln \frac{\phi_1}{x_1} = \ln K_1^{oo} + \frac{V_1^{oo}(P - P_0)}{RT} \]  (8)

Because the saturated vapor pressure of ionic liquid is negligible, it is reasonable to assume P₀ to be zero. Therefore, Eq. (8) can be re-arranged as follows:

\[ \ln \frac{\phi_1}{x_1} = \ln K_1^{oo} + \frac{V_1^{oo}P}{RT} \]  (9)

By plotting and fitting the natural logarithm of the ratio of fugacity to the solubility of CO₂ versus the CO₂ pressure, Henry’s law constant (K₁⁰₀) and the CO₂ partial molar volume (V₁⁰₀) at different temperatures can be obtained.
4. Results and discussions

4.1. Interactions of CO₂ with the ILs

Gurkan et al. reported that FT-IR spectroscopy can be used to distinguish the fractions of physically dissolved and chemically reacted CO₂ since the physically dissolved CO₂ appears cleanly between 2370 and 2310 cm⁻¹ [27]. In this work, ATR FT-IR spectroscopy was used to obtain information about the interactions of CO₂ with [MMIM]DMP, [EMIM]DMP and [EMIM]DEP, which seem to be responsible for the enhanced solubility of CO₂ in phosphate-based ILs. Fig. 1(a) shows the ATR FT-IR spectra of CO₂ stretching band in [MMIM]DMP at various partial pressures of CO₂ ranging from 0 to 4.83 MPa, at 298.15 K. As CO₂ dissolved in the ILs, CO₂ stretching became more and more visible (~2338 cm⁻¹). The stretching of CO₂ progressively decreased in intensity and shifted as the pressure increased. This feature was observed by Kazarian et al. whose investigation showed that the antisymmetric stretching mode of CO₂ dissolved in ionic liquids of [BMIM]PF₆ and [BMIM]BF₄ appears at about 2338 cm⁻¹ [28–30]. CO₂ molecule also exhibits a FT-IR active bending mode, which usually appears around 670 cm⁻¹. When CO₂ is absorbed in a solvent, both the stretching mode and the bending mode could theoretically be observed. This has for instance been reported by Kazarian et al. who investigated CO₂ absorption in [BMIM]PF₆ and [BMIM]BF₄ [28]. In the present study, the absorbance strength related to CO₂ bending mode was very weak (Fig. 1(b)). This feature can be due to the fact that the groups of [MMIM]DMP, [EMIM]DMP and [EMIM]DEP strongly absorb in the region of the bending mode of CO₂, such as the P–O groups in the ILs (Fig. 1(b)).

4.2. Diffusivity of CO₂ in the ILs

The diffusivity of CO₂ in the ILs is crucial to both an understanding of the physical mechanisms controlling transport, as well as an ultimate prediction of the transport rate. The ATR FT-IR spectra of 500 scans for [MMIM]DMP, [EMIM]DMP and [EMIM]DEP at equilibrium were collected under the initial pressure of 1.38 MPa and 298.15 K. CO₂ diffusion coefficients, \( D_{CO_2} \), were calculated by the following equation [31]:

\[
\frac{A}{A_{eq}} = 1 - \frac{4}{\pi} \exp\left(-\frac{\pi^2 D_{CO_2} t}{4l^2}\right)
\]

CO₂ diffusion coefficients in [MMIM]DMP, [EMIM]DMP and [EMIM]DEP under the initial pressure of 1.38 MPa and 298.15 K were 1.53 \( \times 10^{-6} \) cm²/s, 0.95 \( \times 10^{-6} \) cm²/s and 0.42 \( \times 10^{-6} \) cm²/s, respectively. This result indicated that the order of magnitude for the diffusion coefficient of CO₂ in ILs with phosphate-based anion is very close to the values reported for ILs with TF₅N, PF₆, or BF₄ anion (\( 10^{-6} \) cm²/s) [32]. Fig. 2 illustrates the kinetics of CO₂ absorption in the three ILs at 1.38 MPa and 298.15 K. The absorption of CO₂ was complete in about 6 min for [EMIM]DEP, in 4 min for [EMIM]DMP, and in 3 min for [MMIM]DMP. This trend is likely related to the viscosities of the ILs which were 412 mPa s for [EMIM]DEP, 270 mPa s for [EMIM]DMP and 168 mPa s for [MMIM]DMP.

4.3. CO₂-induced swelling of ILs

The CO₂-induced swelling (\( S \)) of ILs at various temperatures and pressures is an important feature in the evaluation of ILs for use in industrial gas treating process. Fig. 1(c) shows ATR FT-IR spectra of C-O in [MMIM]DMP at 298.15 K and
Fig. 2. CO2 diffusion in the three ILs as a function of time at 1.38 MPa and 298.15 K. A/Aeq represents the ratio of the absorbance of CO2 stretching band at any time over the absorbance of CO2 stretching band at equilibrium.

Table 2
List of experimental (\(x_{\text{exp}}^{\text{CO2}}\)) and calculated (\(x_{\text{cal}}^{\text{CO2}}\)) solubilities of CO2 in [MMIM]DMP, their associated CO2-induced swelling (\(S\%\)), relative deviations (RD) as well as experimental mass fraction (\(w_{\text{CO2}}\)) at different temperatures and pressures.

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<th>(x_{\text{exp}}^{\text{CO2}}) (x100)</th>
<th>(x_{\text{cal}}^{\text{CO2}}) (x100)</th>
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<th>(S%)</th>
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\(T = 298.15\) K

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\(ARD\% = 0.81\)

\[RD = \frac{x_{\text{exp}}^{\text{CO2}} - x_{\text{cal}}^{\text{CO2}}}{x_{\text{exp}}^{\text{CO2}}} \times 100\]

\[w_{\text{CO2}} = \frac{x_{\text{exp}}^{\text{CO2}} \times 44}{1000}\]
which then resulted in a decrease in mixture solvent strength. This result indicates that CO₂ is an effective anti-solvent.

4.4. CO₂ capture capacity of ILs

CO₂ capture capacities of [MMIM]DMF, [EMIM]DMF and [EMIM]DEP were calculated using Eq. (3) and listed in Tables 2–4, respectively. As shown in Fig. 4, a comparison of CO₂ solubilities in [MMIM]DMF, [EMIM]DMF and [EMIM]DEP clearly shows that CO₂ capture capacity of these ILs followed the order of [EMIM]DEP > [EMIM]DMF > [MMIM]DMF. For instance, at a pressure of 4.83 MPa and a temperature of 298.15 K, the solubility increased from 0.30 mole fraction for [MMIM]DMF, to 0.35 mole fraction for [EMIM]DMF, to 0.41 mole fraction for [EMIM]DEP. Similar trends were observed at 303.15 K and 313.15 K. The CO₂ solubility in this kind of phosphate-based ILs increased with the increasing alkyl chain length in cation/anion of ILs. These results are supported by the work of Aki et al. who found that CO₂ solubility in [Tf₂N]-based ILs increased with an increase in the alkyl chain length from butyl to octyl [13]. Similarly, Shariati and Peters reported that the solubility of CO₂ in [PF₆]⁻ based ILs increased when the alkyl chain length was increased from ethyl to hexyl [33].

These results may be attributed to the fact that the densities of phosphate-based ILs decreased with the increase of alkyl chain length in IL. So [EMIM]DEP likely had more free volume which in turn allowed for more gas to dissolve. This result further indicates that physical absorption in the phosphate-based ionic liquids played a significant role for the solubility of CO₂.

4.5. Henry’s law constants of CO₂ in phosphate-based ILs

The solubility data of CO₂ in ILs can be calculated using the Krichevsky–Kasarnovsky (K–K) and Span–Wagner equations [34], and the calculated results are listed in Tables 2–4. In Fig. 5, the logarithm of the ratio of fugacity to the
The solubilities of CO₂ in [MMIM]DMP is plotted versus the pressure. Using this plot, the Henry's constants at zero pressure were obtained. The Henry's constants of [MMIM]DMP and [EMIM]DEP at 313.15 K were 10.54 MPa and 6.95 MPa, respectively, which are in good agreement with the values of 10.66 MPa and 6.94 MPa [35]. For [EMIM]DMP, the Henry's constant at the same conditions was 9.13 MPa, which was between the values of [MMIM]DMP and [EMIM]DEP. The Henry's constants of other ionic liquids with the same [EMIM]⁺ cation as well as that of [BMIM]PF₆ have already been reported [36]. The Henry's constants at 298.15 K followed this order: [EMIM]Tf₂N < [EMIM]DEP < [BMIM]PF₆ < [EMIM]DMP < [EMIM]TfO < [EMIM]DCA < [EMIM]BF₄ (as shown in Fig. 6). The larger CO₂ solubility of [EMIM]DEP compared to the other two ILs suggests that ester-containing anions may be advantageous to CO₂ capture and/or that phosphate-containing anions (like DEP and DMP) may favor CO₂ capture.

5. Conclusions

In this study, ATR FT-IR spectroscopy was used to determine the CO₂ capture capacity and CO₂-induced swelling of phosphate-based ionic liquids over the temperature range from 298.15 to 313.15 K and pressures up to 4.83 MPa. CO₂ capture mechanism in the three ILs studied in this work was determined as physical absorption. With the increase of the alkyl chain length in ILs, the free volume of ILs increased, which caused the CO₂ solubility to increase and the diffusion coefficient to decrease. Over the temperature range from 298.15 to 313.15 K, Henry's law constants of CO₂ in [MMIM]DMP ranged from 6.66 to 10.54 MPa, those in [EMIM]DMP ranged from 6.02 to 9.13 MPa, and those in [EMIM]DEP ranged from 4.90 to 6.95 MPa, following an inverse relationship with solubility.

Conflict of interest

The authors declared that they have no conflicts of interest to this work.

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Symbols used

- \( A^0 \) absorbance without CO₂ pressure
- \( A \) absorbance with CO₂ pressure
- \( c \) concentration (g cm\(^{-3}\))
- \( d_e \) arithmetical mean between the effective path length for perpendicular and parallel polarization
- \( d_e^0 \) effective path length without CO₂ pressure
- \( D_{CO₂} \) diffusion coefficient of CO₂ in ionic liquids
- \( f_i \) fugacity of CO₂ in the gas phase at system temperature and pressure
- \( f_i^G \) fugacity of carbon dioxide in gas phase
- \( f_i^L(p_l) \) fugacity of carbon dioxide in liquid phase
- \( K_H \) Henry's law constant on mole-fraction scale of CO₂ in ionic liquid at saturated vapor pressure of ionic liquid
- \( K_H^0 \) Henry's law constant at zero pressure
- \( l \) the thick of ionic liquid film (mm)
- \( m \) CO₂ capture capacity (mol kg\(^{-1}\))
- \( M \) molecular weight of CO₂ (g mol\(^{-1}\))
- \( M_{IL} \) molecular weight of ionic liquid (g mol\(^{-1}\))
- \( P \) total pressure (MPa)
- \( P_s^2 \) saturated vapor pressure of ionic liquid
- \( R \) universal gas constant
degree of swelling

\( t \)  
temperature (K)

\( \mathbf{V}_1 \)  
the partial molar volume of CO\(_2\) in ionic liquid (m\(^3\) mol\(^{-1}\))

\( \mathbf{V}_1^\infty \)  
partial molar volume of CO\(_2\) at dilution condition in liquid phase (m\(^3\) mol\(^{-1}\))

\( \lambda_1^{\text{calc}} \)  
calculated mole fraction

\( \lambda_1^{\text{exp}} \)  
experimental mole fraction

\( \rho \)  
density (g cm\(^{-3}\))

\( \phi_1 \)  
fugacity coefficient

\( \varepsilon \)  
a constant related to the optical properties of the absorbing substance (1.0 × 10\(^6\) cm\(^2\) mol\(^{-1}\))

References